drops of preproduct are introduced and wherein said gaseous medium carries out acceleratively a crystallization status of said preproduct by maintaining said drops of said preproduct above a temperature of 100° C and below its melting point for a limited period of time until a crystallization of said drops is finished on their surface.

21. (New) The method according to claim 20, characterized in that air is used as said gaseous medium.

22. (New) The method according to claim 20, characterized in that an atmosphere poor of oxygen is used as a said gaseous medium.

23. (New) The method according to claim 20, characterized in that inert gas is used as said gaseous medium.

24. (New) The method according to claim 20, characterized in that nitrogen is used as said gaseous medium.

25. (New) The method according to any one of the previous claims, characterized in that said gaseous medium is directed in a counterflow of a drop section of said drops of the preproduct.

26. (New) The method according to claim 25, characterized in that said gaseous medium is tempered with said drop section of said drops of said preproduct and introduced at the lowest point of said drop section.

27. (New) The method according to claim 26, characterized in that the tempering of said gaseous medium is performed by heat exchanger and that said gaseous medium is conducted in a recycled process.

28. (New) The method according to claim 20, characterized in that said

molten preproduct is formed to drops by a vibrational stimulation.

29. (New) The method according to claim 20, characterized in that said preproduct is formed to drops having an intrinsic viscosity in the range between 0.05 to 0.3 cm^3/g.

30. (New) The method according to claim 20, characterized in that said preproduct is formed to drops which a diameter is in the range of the double of a nozzle diameter for more than 80 weight-% and which diameter is below the diameter of said nozzle for less than 3 weight-% and which diameter is larger than three times said nozzle diameter for less than 10 weight-% of the drops of said preproduct.

31. (New) The method according to claim 20, characterized in that a dust particle ratio is present during formation of drops which is less than 1 weight-% of said drops of said preproduct.

32. (New) The method according to claim 20, characterized in that a low viscosity preproduct having an intrinsic viscosity lower than 0.15 is formed to drops in an environment enclosing fine polyester particles, so that a coating of said drops at their surface takes place with said polyester particles which enhance the crystallization and avoid an adhesion of the solidified drops.

33. (New) An apparatus for performing the methods according to claim 20 wherein the apparatus comprises:

a nozzlehead (1) which forms by vibrational stimulation of the melt (3) drop-shaped pellets (3) having a diameter of 0.3 to 3 mm of a preproduct,

a drop tower (4) wherein said preproduct of drops is temperable in a

counterflow of a gaseous medium,

a heat exchanger (5) positioned at the bottom part of said drop tower (4) and wherein said gaseous medium is heated or cooled to control a homogenous high entrance flow temperature,

a fan means (6) which accelerates the gaseous medium in the drop tower (4) up to a predetermined flow velocity and

a recycle line (7) which conducts the gaseous medium to said heat exchanger (5) after departing from the drop tower (4).

34. (New) The apparatus according to claim 33, characterized in that the nozzlehead (1) comprises nozzle openings (8) which are vertically adjusted and which ensure a drop forming in vertical direction by vibrational stimulation of the melt (2).

35. (New) The apparatus according to claim 33 or 34, characterized in that said heat exchanger (5) controls the temperature of the gaseous medium to an entrance temperature of larger than 30° C and smaller or equal to 120° C.

36. (New) The apparatus according to claim 33, characterized in that said fan means (6) is adjustable to a flow velocity from 0.3 to 1 m/s for said gaseous medium within the drop tower (4).

37. (New) The apparatus according to one of the claim 33, characterized in that said drop tower (4) comprises a drop section (9) from 10 to 20 m for said drops of said preproduct.